

\*\*\*\*\*  
USACE / NAVFAC / AFCEA UFGS-11377 (November 2003)  
-----  
Preparing Activity: USACE Superseding  
UFGS-11377 (June 2001)

## UNIFIED FACILITIES GUIDE SPECIFICATIONS

References are in agreement with UMRL dated 25 June 2004

Latest change indicated by CHG tags

\*\*\*\*\*

### SECTION TABLE OF CONTENTS

#### DIVISION 11 - EQUIPMENT

#### SECTION 11377

#### ADVANCED OXIDATION PROCESSES (AOP)

11/03

#### PART 1 GENERAL

- 1.1 REFERENCES
- 1.2 MEASUREMENT AND PAYMENT
- 1.3 SUBMITTALS
- 1.4 SYSTEM DESCRIPTION
  - 1.4.1 Design Requirements
  - 1.4.2 Performance Requirements
  - 1.4.3 Treatability Testing
- 1.5 QUALIFICATIONS
  - 1.5.1 Contractor
  - 1.5.2 Ultraviolet (UV) Oxidation System Supplier
  - 1.5.3 Manufacturer's Representative
  - 1.5.4 Welding
- 1.6 REGULATORY REQUIREMENTS
- 1.7 STANDARD PRODUCTS
- 1.8 NAMEPLATES
- 1.9 PRE-SUBMITTAL CONFERENCE
- 1.10 DELIVERY AND STORAGE
- 1.11 PROJECT/SITE CONDITIONS

#### PART 2 PRODUCTS

- 2.1 MATERIALS
  - 2.1.1 Plates, Shapes and Bars
  - 2.1.2 Pipe and Fittings
    - 2.1.2.1 Stainless Steel Pipe
    - 2.1.2.2 Polyvinyl Chloride (PVC) Pipe
    - 2.1.2.3 Polytetrafluoroethylene (PTFE) Pipe and Tubing
    - 2.1.2.4 Polyvinylidene Fluoride (PVDF) Pipe and Tubing
    - 2.1.2.5 Copper Pipe
  - 2.1.3 Pipe Hangers and Supports
  - 2.1.4 Stainless Steel Gas Tubing and Fittings
  - 2.1.5 Valves

- 2.1.5.1 Liquid Oxygen (LOX)
- 2.1.5.2 Gate
- 2.1.5.3 Ball
- 2.1.5.4 Check
- 2.1.6 Injectors
- 2.1.7 Diffusers
- 2.1.8 Couplings
- 2.1.9 Insulating Joints
- 2.1.10 In Pipeline Static Mixers
- 2.1.11 Bolts, Nuts, Anchors and Fasteners
- 2.2 MANUFACTURED UNITS
  - 2.2.1 Swing Adsorption Oxygen Generation System
  - 2.2.2 Liquid Oxygen (LOX) Storage and Supply System
    - 2.2.2.1 LOX Storage Tanks
    - 2.2.2.2 Vaporizers
    - 2.2.2.3 Regulators
  - 2.2.3 Ozone Generator Air Feed System
  - 2.2.4 Ozone Generator System
    - 2.2.4.1 Ozone Generator Vessels
    - 2.2.4.2 Dielectric Tubes
  - 2.2.5 Ozone Destruct System
  - 2.2.6 Hydrogen Peroxide System
  - 2.2.7 Redox Potential Meter
  - 2.2.8 pH Probe
  - 2.2.9 Ozone Monitors
    - 2.2.9.1 Vapor Phase
    - 2.2.9.2 Liquid Phase
  - 2.2.10 Temperature Sensors
  - 2.2.11 Compressors
  - 2.2.12 Blowers
  - 2.2.13 Dew Point Monitor
  - 2.2.14 Pressure Gauges
  - 2.2.15 Sampling Ports
  - 2.2.16 Gas Flow Meters
  - 2.2.17 Level Monitoring
  - 2.2.18 Reactor Vessel
- 2.3 ELECTRICAL
  - 2.3.1 Motors
  - 2.3.2 Local Controls and Panels
  - 2.3.3 Ultraviolet Equipment Electrical Requirements
- 2.4 AOP CONTROL SYSTEM
  - 2.4.1 Ozonation Control System
  - 2.4.2 Hydrogen Peroxide Feed
  - 2.4.3 Alarms and Interlocks
    - 2.4.3.1 AOP System
    - 2.4.3.2 Metering Pump
    - 2.4.3.3 Hydrogen Peroxide Tank
    - 2.4.3.4 Ozone System
    - 2.4.3.5 Gas Feed System
    - 2.4.3.6 Ozone Destruct System
    - 2.4.3.7 Cooling Water System
    - 2.4.3.8 Metering Accuracy
    - 2.4.3.9 Ground Fault
- 2.5 SPECIAL EQUIPMENT AND TOOLS

## PART 3 EXECUTION

- 3.1 EXAMINATION
- 3.2 PREPARATION

|          |   |
|----------|---|
| 3.3      | PIPES, VALVES, FITTINGS AND APPURTENANCES |
| 3.4      | ELECTRICAL WORK                           |
| 3.5      | TOOLS                                     |
| 3.6      | PAINTING/CORROSION PROTECTION             |
| 3.7      | CHEMICALS                                 |
| 3.8      | WELDING                                   |
| 3.9      | SAMPLING AND ANALYSIS                     |
| 3.10     | FIELD TESTS AND INSPECTIONS               |
| 3.10.1   | AOP Reactor Vessel                        |
| 3.10.2   | Diffuser or Injector System               |
| 3.10.3   | Leak Testing                              |
| 3.10.4   | Control Panel                             |
| 3.10.5   | Ozone Generation System                   |
| 3.11     | MANUFACTURER'S SERVICES                   |
| 3.12     | FIELD TRAINING                            |
| 3.13     | MAINTENANCE                               |
| 3.13.1   | Maintenance Service                       |
| 3.13.2   | Extra Materials                           |
| 3.13.2.1 | Lamps                                     |
| 3.13.2.2 | Spare Parts                               |
| 3.14     | POSTING FRAMED INSTRUCTIONS               |

-- End of Section Table of Contents --

\*\*\*\*\*  
USACE / NAVFAC / AFCESA UFGS-11377 (November 2003)  
-----  
Preparing Activity: USACE Superseding  
UFGS-11377 (June 2001)

## UNIFIED FACILITIES GUIDE SPECIFICATIONS

References are in agreement with UMRL dated 25 June 2004

Latest change indicated by CHG tags

\*\*\*\*\*

### SECTION 11377

#### ADVANCED OXIDATION PROCESSES (AOP) 11/03

\*\*\*\*\*

NOTE: This guide specification covers the requirements for liquid phase advanced oxidation processes using titanium dioxide or hydrogen peroxide and/or ozone with or without ultraviolet light.

Comments and suggestions on this guide specification are welcome and should be directed to the technical proponent of the specification. A listing of technical proponents, including their organization designation and telephone number, is on the Internet.

Recommended changes to a UFGS should be submitted as a Criteria Change Request (CCR).

Use of electronic communication is encouraged.

Brackets are used in the text to indicate designer choices or locations where text must be supplied by the designer.

\*\*\*\*\*

## PART 1 GENERAL

### 1.1 REFERENCES

\*\*\*\*\*

NOTE: Issue (date) of references included in project specifications need not be more current than provided by the latest guide specification. Use of SpecsIntact automated reference checking is recommended for projects based on older guide specifications.

\*\*\*\*\*

The publications listed below form a part of this specification to the extent referenced. The publications are referred to within the text by the basic designation only.

AMERICAN WELDING SOCIETY (AWS)

|                |  |
|----------------|--|
| AWS B2.1       | (2000) Welding Procedure and Performance Qualification |
| AWS D1.1/D1.1M | (2002) Structural Welding Code - Steel                 |

ASME INTERNATIONAL (ASME)

|                       |  |
|-----------------------|--|
| ASME B16.18           | (2002) Cast Copper Alloy Solder Joint Pressure Fittings  |
| ASME B16.22           | (2002) Wrought Copper and Copper Alloy Solder Joint Pressure Fittings                              |
| ASME B16.5            | (1996) Pipe Flanges and Flanged Fittings   |
| ASME B16.9            | (2001) Factory-Made Wrought Steel Buttwelding Fittings   |
| ASME B19.3            | (1991) Safety Standard for Compressors for Process Industries                                      |
| ASME B31.1            | (2001) Power Piping  |
| ASME B40.100          | (2000) Pressure Gauges and Gauge Attachments   |
| ASME BPVC SEC IX      | (2001) Boiler and Pressure Vessel Code; Section IX, Welding and Brazing Qualifications             |
| ASME BPVC SEC VIII D1 | (2001) Boiler and Pressure Vessel Code; Section VIII, Pressure Vessels Division 1 - Basic Coverage |

ASTM INTERNATIONAL (ASTM)

|                   |  |
|-------------------|--|
| ASTM A 182/A 182M | (2002) Forged or Rolled Alloy-Steel Pipe Flanges, Forged Fittings, and Valves and Parts for High-Temperature Service |
| ASTM A 269        | (2002a) Seamless and Welded Austenitic Stainless Steel Tubing for General Service                                    |
| ASTM A 276        | (2003) Stainless Steel Bars and Shapes   |
| ASTM A 312/A 312M | (2002) Seamless and Welded Austenitic Stainless Steel Pipes  |
| ASTM A 36/A 36M   | (2003a) Carbon Structural Steel  |
| ASTM A 403/A 403M | (2003a) Wrought Austenitic Stainless Steel Piping Fittings   |
| ASTM A 53/A 53M   | (2002) Pipe, Steel, Black and Hot-Dipped, Zinc-Coated, Welded and Seamless   |

|                   |   |
|-------------------|---|
| ASTM A 774/A 774M | (2002) As-Welded Wrought Austenitic Stainless Steel Fittings for General Corrosive Service at Low and Moderate Temperatures |
| ASTM A 778        | (2001) Welded, Unannealed Austenitic Stainless Steel Tubular Products   |
| ASTM B 209        | (2002a) Aluminum and Aluminum-Alloy Sheet and Plate   |
| ASTM B 209M       | (2002a) Aluminum and Aluminum-Alloy Sheet and Plate (Metric)  |
| ASTM B 32         | (2003) Solder Metal   |
| ASTM B 88         | (2002) Seamless Copper Water Tube   |
| ASTM B 88M        | (1999) Seamless Copper Water Tube (Metric)  |
| ASTM D 1710       | (2002) Extruded and Compression Molded Polytetrafluoroethylene (PTFE) Rod and Heavy-Walled Tubing                           |
| ASTM D 1785       | (1999) Poly(Vinyl Chloride) (PVC) Plastic Pipe, Schedules 40, 80, and 120   |
| ASTM D 2241       | (2000) Poly(Vinyl Chloride) (PVC) Pressure-Rated Pipe (SDR Series)  |
| ASTM D 2564       | (2002) Solvent Cements for Poly(Vinyl Chloride) (PVC) Plastic Piping Systems  |
| ASTM D 3222       | (1999) Unmodified Poly(Vinylidene Fluoride) (PVDF) Molding Extrusion and Coating Materials                                  |
| ASTM F 593        | (2002) Stainless Steel Bolts, Hex Cap Screws, and Studs   |

#### COMPRESSED GAS ASSOCIATION (CGA)

|           |   |
|-----------|---|
| CGA G-4.1 | (1996) Cleaning Equipment for Oxygen Service  |
| CGA G-4.4 | (1993) Industrial Practices for Gaseous Oxygen Transmission and Distribution Piping Systems |
| CGA HB    | (1999) Handbook of Compressed Gases   |

#### ISA - THE INSTRUMENTATION, SYSTEMS AND AUTOMATION SOCIETY (ISA)

|          |   |
|----------|---|
| ISA S5.1 | (1984; R 1992) Instrumentation Symbols and Identification |
|----------|---|

MANUFACTURERS STANDARDIZATION SOCIETY OF THE VALVE AND FITTINGS  
INDUSTRY (MSS)

MSS SP-43 (1991; R 2001) Wrought Stainless Steel  
Butt-Welding Fittings

MSS SP-58 (2002) Pipe Hangers and Supports -  
Materials, Design and Manufacture

MSS SP-69 (2002) Pipe Hangers and Supports -  
Selection and Application

NATIONAL ELECTRICAL MANUFACTURERS ASSOCIATION (NEMA)

NEMA 250 (2003) Enclosures for Electrical Equipment  
(1000 Volts Maximum)

NEMA ICS 6 (1993; R 2001) Industrial Control and  
Systems: Enclosures

NATIONAL FIRE PROTECTION ASSOCIATION (NFPA)

NFPA 50 (2001) Bulk Oxygen Systems at Consumer  
Sites

NFPA 70 (2002) National Electrical Code

1.2 MEASUREMENT AND PAYMENT

Measurement and payment requirements shall be as identified in the Payment  
Schedule of the Bid Form.

1.3 SUBMITTALS

\*\*\*\*\*

NOTE: Submittals must be limited to those necessary  
for adequate quality control. The importance of an  
item in the project should be one of the primary  
factors in determining if a submittal for the item  
should be required.

A "G" following a submittal item indicates that the  
submittal requires Government approval. Some  
submittals are already marked with a "G". Only  
delete an existing "G" if the submittal item is not  
complex and can be reviewed through the Contractor's  
Quality Control system. Only add a "G" if the  
submittal is sufficiently important or complex in  
context of the project.

For submittals requiring Government approval on Army  
projects, a code of up to three characters within  
the submittal tags may be used following the "G"  
designation to indicate the approving authority.  
Codes for Army projects using the Resident  
Management System (RMS) are: "AE" for  
Architect-Engineer; "DO" for District Office  
(Engineering Division or other organization in the  
District Office); "AO" for Area Office; "RO" for

Resident Office; and "PO" for Project Office. Codes following the "G" typically are not used for Navy projects.

Submittal items not designated with a "G" are considered as being for information only for Army projects and for Contractor Quality Control approval for Navy projects.

\*\*\*\*\*

Government approval is required for submittals with a "G" designation; submittals not having a "G" designation are [for Contractor Quality Control approval.] [for information only. When used, a designation following the "G" designation identifies the office that will review the submittal for the Government.] The following shall be submitted in accordance with Section 01330 SUBMITTAL PROCEDURES:

#### SD-02 Shop Drawings

Shop Drawings[; G][; G, [\_\_\_\_]]  
AOP System[; G][; G, [\_\_\_\_]]  
Air Preparation System[; G][; G, [\_\_\_\_]]  
Oxygen Generation System[; G][; G, [\_\_\_\_]]  
LOX Storage System[; G][; G, [\_\_\_\_]]  
Ozone Generation System[; G][; G, [\_\_\_\_]]  
Reactor Vessel[; G][; G, [\_\_\_\_]]  
Metering Pump[; G][; G, [\_\_\_\_]]  
Local Controls and Panels[; G][; G, [\_\_\_\_]]  
Liquid Process Tank[; G][; G, [\_\_\_\_]]  
Maintenance[; G][; G, [\_\_\_\_]]

Drawings showing shop and erection details and chemical application locations; including cuts, codes, connections, holes, bolts, welds, anchorage, installation details, wiring diagrams, schematic diagrams, component identification tables and directory, and clearances for maintenance and operations.

#### SD-03 Product Data

AOP System[; G][; G, [\_\_\_\_]]

a. Manufacturer's descriptive and technical literature; performance charts and curves, catalog cuts for specified equipment including: instrumentation and controls; capacities and pressure drop; model number; and installation instructions.

b. Materials of construction; inlet and outlet pipe sizes; power demand requirements; and ozone generator cooling water flow rate.

c. Spare parts data for each piece of equipment, current unit prices and source of supply.

d. Manufacturer's descriptive and technical literature; performance charts and curves, catalog cuts for specified equipment including: instrumentation and controls; capacities and pressure drop; model number; and installation instructions.

e. Materials of construction; inlet and outlet pipe sizes;



power demand requirements; and ozone generator cooling water flow rate.

f. Spare parts data for each piece of equipment, current unit prices and source of supply.

Calculations[; G][; G, [\_\_\_\_\_]]

a. Headloss calculations through the process units at the design flow rate, including headloss calculations for associated compressed air and pumping systems.

b. Oxidant demand and subsequent AOP unit sizing.

c. Electrical usage rate.

d. Removal performance and material mass balance.

e. Chemical feed requirements and equipment sizing.

f. Diffuser system layout, mass transfer calculations.

Commissioning/Demonstration Plan[; G][; G, [\_\_\_\_\_]]

The Contractor shall submit a plan detailing the sampling locations, frequency, analytical protocols, and duration which will ensure the equipment complies with the standards indicated. The plan shall be submitted to the contracting officer [\_\_\_\_\_] [30] days prior to equipment start up. The Contractor shall coordinate work within this section with other sections to ensure upstream and downstream unit processes are complete and operational prior to startup/commissioning the AOP unit.

a. Headloss calculations through the process units at the design flow rate, including headloss calculations for associated compressed air and pumping systems.

b. Oxidant demand and subsequent AOP unit sizing.

c. Electrical usage rate.

d. Removal performance and material mass balance.

e. Chemical feed requirements and equipment sizing.

f. Diffuser system layout, mass transfer calculations.

The Contractor shall submit a plan detailing the sampling locations, frequency, analytical protocols, and duration which will ensure the equipment complies with the standards indicated. The plan shall be submitted to the contracting officer [\_\_\_\_\_] [30] days prior to equipment start up. The Contractor shall coordinate work within this section with other sections to ensure upstream and downstream unit processes are complete and operational prior to startup/commissioning the AOP unit.

Manufactured Units

Wiring and control diagrams, systems layouts and isometrics,

component identification tables, instructions, and other sheets, prior to posting. Condensed operating instructions explaining preventative maintenance procedures, methods of checking the system for safe operation, making adjustments, and procedures for safely starting and stopping the system shall be prepared in typed form, framed and posted beside the diagrams.

Performance Requirements[; G][; G, [\_\_\_\_]]  
Qualifications[; G][; G, [\_\_\_\_]]

A statement by the equipment manufacturer listing any exception to or deviations from the contract drawings and specifications. Written evidence that equipment and accessories are a product of a qualified and experienced manufacturer. Statement indicating the system is capable of treating the wastes to the levels identified. A statement indicating the operators designated to train the on site operators have been trained to operate the installed equipment.

#### SD-06 Test Reports

Performance Requirements[; G][; G, [\_\_\_\_]]

a. Performance tests results indicating temperature rise through the reactor, oxidant dosage, detention time, catalyst dosage, ultraviolet light dosage, ambient gas monitoring results, and treatment system off gas monitoring and destruction results, equipment and analytical testing methods used, and removal of constituents identified in paragraph Performance Requirements stated in mass/unit volume treated relative to the influent concentration.

b. Report in booklet form, upon completion of the installed system. Test report shall include field tests performed to adjust each component and field tests conducted to prove compliance with the specified performance criteria. Test report shall indicate the recommended position of the controls.

#### SD-07 Certificates

##### AOP System

Manufacturer's certificates stating that the equipment meets the specified requirements, and has been installed in accordance with the equipment manufacturer's requirements.

##### Field Training

Certificates indicating the designated personnel have received training specified and have successfully operated the installed AOP equipment.

#### SD-10 Operation and Maintenance Data

AOP System[; G][; G, [\_\_\_\_]]  
Maintenance[; G][; G, [\_\_\_\_]]

[Six] [\_\_\_\_] complete copies of operating instructions outlining the step-by-step procedures required for system

start-up, operation and shutdown, routine maintenance, potential breakdowns and repairs, and troubleshooting. The instructions shall include drawings and schematics of the system as installed. The instructions shall include the manufacturer's name, model number, service manual parts list and brief description of all equipment and their basic operating features. The instructions shall include, but not be limited to, the following:

a. System layout showing piping, valves and controls, process flow diagrams, piping and instrumentation diagrams with all valves, meters, and similar units identified.

b. Approved wiring and control diagrams prepared in accordance with ISA S5.1 including a drawing index, legend and symbols list, and abbreviations and identifiers.

c. A control sequence describing startup, how to make adjustments to the equipment during operation, standard and emergency shutdown procedures.

d. Operating and maintenance instructions for each piece of equipment, including lubrication instructions and other periodic maintenance and inspection information as well as trouble shooting guides.

e. Manufacturer's bulletins, cut sheets and descriptive data, parts lists, and recommended spare parts, and sources of supply for all major pieces of equipment.

#### 1.4 SYSTEM DESCRIPTION

\*\*\*\*\*

NOTE: This paragraph should be edited to identify the appropriate contaminants of concern as well as those parameters which potentially inhibit the process as indicated in ETL 1110-1-161 ULTRAVIOLET/CHEMICAL OXIDATION dated 29 March 96.

Effluent limitations are generally dictated by regulatory requirements. List the performance requirements in this specification and cross reference Section 01450A CHEMICAL DATA QUALITY CONTROL for the analytical and sampling protocols.

If this specification is used as part of a Request for Proposals, the designer should identify maximum values for power and oxidant usage based on bench or pilot studies and include this information in Paragraph Performance Requirements.

\*\*\*\*\*

The AOP shall include all items necessary to provide a complete system for removal of those chemicals identified below to the levels indicated. Equipment includes, but is not limited to, AOP contact vessels, lamps when required, piping to units upstream and downstream of the contact vessels, oxidant feed system, gas emission treatment, controls, accessories and equipment to provide complete and functional system within the limits identified. Analytical and sampling protocols shall be as specified in Section 01450A CHEMICAL DATA QUALITY CONTROL.

#### 1.4.1 Design Requirements

|   |  |
|---|--|
| Minimum equipment life                          | [20] [_____] years                                 |
| Max. equipment dimensions                       | [As shown on the drawings] [_____] [_____] [_____] |
| Maximum AOP reactor operating pressure          | [_____] kPa psi                                    |
| Reactor inlet pipe diam.                        | [_____] mm inches                                  |
| Reactor outlet pipe diam.                       | [_____] mm inches                                  |
| Max. cooling water temp.                        | [_____] degrees C F                                |
| Max. cooling water flow rate                    | [_____] L/s gpm                                    |
| Max. AOP influent flow rate                     | [_____] L/s gpm                                    |
| Minimum reactor vessel Detention time           | [_____] minutes                                    |
| Max. liquid temperature rise Across AOP reactor | [_____] degrees C F                                |

#### 1.4.2 Performance Requirements

##### a. Influent characteristics:

##### Inorganic Constituent Concentration

|   |              |
|---|--------------|
| Iron (Fe <sup>2+</sup> )                              | [_____] mg/L |
| HCO <sub>3</sub> <sup>-</sup> (as CaCO <sub>3</sub> ) | [_____] mg/L |
| [_____]   | [_____] mg/L |

##### Organic Constituent Concentration

|                            |               |
|----------------------------|---------------|
| [_____]                    | [_____] ug/L  |
| pH                         | [_____] units |
| Total Organic Carbon (TOC) | [_____] mg/L  |

##### b. Effluent requirements:

##### Organic Constituent Concentration

|                              |                     |
|------------------------------|---------------------|
| [_____]                      | [_____] ug/L        |
| Total Organic Carbon (TOC)   | [_____] mg/L        |
| pH                           | [_____] units       |
| Maximum effluent temperature | [_____] degrees C F |

c. Efficiency factors:

|                         |              |
|-------------------------|--------------|
| Ozone usage             | [_____] mg/L |
| Hydrogen peroxone usage | [_____] mg/L |
| Power consumption       | [_____] kW/L |
| [Catalyst usage]        | [_____] mg/L |

1.4.3 Treatability Testing

\*\*\*\*\*  
NOTE: This paragraph should be deleted if previous  
treatability studies have not been conducted. The  
system parameters used during the treatability study  
may not duplicate the system proposed by the  
Contractor. The previous treatability studies  
should be properly documented to include the  
information contained in ETL 1110-1-161.  
\*\*\*\*\*

The previously conducted treatability study information contained in  
Appendix [\_\_\_\_\_] is provided for the Contractor's information. The study  
results indicate [ultraviolet oxidation] [peroxone] [\_\_\_\_\_] is capable of  
meeting the criteria in paragraph Performance Requirements above. The  
Contractor shall evaluate the applicability and adequacy of the  
treatability studies and results provided. If deemed necessary by the  
Contractor, additional studies may be performed at the Contractor's expense  
to confirm the previously conducted treatability study and results. Based  
on the Contractor's own interpretation of the previous studies and results,  
and additional studies and results the Contractor elects to perform, the  
Contractor shall provide a full scale treatment plant which meets the  
requirements identified.

1.5 QUALIFICATIONS

\*\*\*\*\*  
NOTE: Designer should edit the subsequent  
paragraphs and remove requirements not applicable to  
the project.  
\*\*\*\*\*

1.5.1 Contractor

Contractor shall have a minimum of [3] [\_\_\_\_\_] years of experience in the  
construction of water, wastewater, industrial wastewater, or hazardous and  
toxic waste water treatment facilities. The Contractor shall be  
responsible for installation and start-up of the AOP equipment supplied, as  
well as operator training.

1.5.2 Ultraviolet (UV) Oxidation System Supplier

Equipment provided must duplicate equipment that has been in satisfactory  
service for a minimum of [2] [\_\_\_\_\_] years prior to bid opening. The UV  
oxidation system supplier shall be responsible for furnishing a complete  
prepackaged system. The supplier need not manufacture the entire system,  
but shall coordinate the selection, assembly, installation, and testing of  
the entire system as specified.

### 1.5.3 Manufacturer's Representative

Services of a qualified manufacturer's field representative experienced in the installation, adjustment, and operation of the equipment furnished and who has complete knowledge of the proper operation and maintenance of the system shall be provided as specified.

### 1.5.4 Welding

Welding shall be done following qualified procedures, using performance qualified welders and welding operators. The Contractor shall furnish a copy of qualified procedures and a list of names and identification symbols of qualified welders and welding operators to the Contracting Officer prior to beginning any work on the AOP equipment.

## 1.6 REGULATORY REQUIREMENTS

The AOP system shall conform to all federal, state, regional, and local regulations concerning chemical storage, air, noise and water pollution control requirements.

## 1.7 STANDARD PRODUCTS

Materials and equipment shall be the standard products of a manufacturer regularly engaged in the manufacture of such products and shall essentially duplicate items that have been in satisfactory use for at least 2 years prior to bid opening. Equipment shall be supported by a service organization that is, in the opinion of the Contracting Officer, reasonably convenient to the site.

## 1.8 NAMEPLATES

Each major item of equipment shall have the manufacturer's name, address, type or style, model or serial number, and catalog number on a plate secured to the item of equipment. Nameplates shall be provided for, but not limited to, each contact vessel, pumps, motors, oxidant equipment and accessories, and electrical components such as transformers.

## 1.9 PRE-SUBMITTAL CONFERENCE

The Contractor shall assemble the primary process designer, AOP equipment and major component suppliers, electrical and mechanical subcontractors, and major component manufacturer's representatives at [the construction site] [\_\_\_\_\_] prior to preparation of the Contractor's AOP submittal for government approval. This meeting is intended to ensure that facility construction is properly scheduled; power, control, plumbing, space interfaces are verified; and responsibilities coordinated among subcontractor's and suppliers and reflected on the Contractor's AOP submittals.

## 1.10 DELIVERY AND STORAGE

\*\*\*\*\*

**NOTE: Designer should coordinate with the Contracting Officer and user to determine appropriate locations for equipment storage. Identify unusual requirements either here or on the drawings.**

\*\*\*\*\*

Equipment shall be delivered free of structural or other damage and placed in storage protected from structural damage, the weather, excessive humidity and excessive temperature variation; and dirt, dust, or other contaminants that could otherwise damage its components. Storage shall be in accordance with the manufacturer's requirements.

#### 1.11 PROJECT/SITE CONDITIONS

After becoming familiar with all details of the work, the Contractor shall verify all dimensions in the field, and shall advise the Contracting Officer of any discrepancy before performing the work.

### PART 2 PRODUCTS

#### 2.1 MATERIALS

##### 2.1.1 Plates, Shapes and Bars

Steel shall conform to ASTM A 36/A 36M; stainless steel shall conform with ASTM A 276, type 316.

##### 2.1.2 Pipe and Fittings

\*\*\*\*\*

**NOTE: Designer should coordinate with the oxidizer equipment suppliers to coordinate piping and gasket material requirements.**

\*\*\*\*\*

Gasket materials for pipe and fittings shall be silicon, or teflon unless otherwise shown or specified.

##### 2.1.2.1 Stainless Steel Pipe

- a. Pipe 100 mm 4 inch and larger shall conform to ASTM A 312/A 312M, Schedule 40, Type 316L with maximum carbon content of 0.04 percent. Flanged fittings shall conform to ASME B16.5, F316L Class 150 with 2 mm 1/16 inch minimum thickness silicon, teflon, expanded PTFE, PVDF, or viton gaskets. Butt weld fittings shall conform to ASTM A 403/A 403M and MSS SP-43, Grade 316L, Schedule 10S with full penetration welds.
- b. Pipe less than 100 mm 4 inch shall be type TP316, and conform to ASTM A 312/A 312M Schedule 80S for threaded joints, and Schedule 40S for welded joints. Flanged joints shall conform to ASTM A 182/A 182M, F316 or F316L, Class 150; dimensions and drilling shall be in accordance with ASME B16.5 with 2 mm 1/16 inch minimum thickness silicone, teflon, expanded PTFE, PVDF, or viton gaskets. Butt weld fittings shall conform to ASTM A 774/A 774M, ASTM A 778, and ASME B16.9.
- c. Liquid tubing 10 mm 3/8 inch and smaller shall be seamless austenitic stainless steel and shall conform to ASTM A 269, Type TP316. Wall thickness shall be adequate for the pressure required. Fittings shall be compression type made from bar stock material conforming to ASTM A 276, Type 316, with forgings conforming with ASTM A 182/A 182M, Type 316. Assemblies shall

consist of tube, fittings and components of one manufacturer.

#### 2.1.2.2 Polyvinyl Chloride (PVC) Pipe

PVC pipe and fittings less than 100 mm 4 inch diameter shall be in accordance with ASTM D 1785 or ASTM D 2241. PVC pipe and fittings 100 mm 4 inch in diameter and larger shall be in accordance with ASTM D 2241. Pipe and joints shall be rated for a working pressure of [\_\_\_\_\_] kPa psi. Solvent cement joints shall conform to the requirements of ASTM D 2564. Flanged joint diameter and drilling shall conform to ASME B16.5, Class 150.

#### 2.1.2.3 Polytetrafluoroethylene (PTFE) Pipe and Tubing

Pipe and fittings shall conform to ASTM D 1710, Type I, Grade 1, Class A, with PTFE compression type fittings. Pipe, tubing and associated fittings shall be rated for a minimum working pressure of [\_\_\_\_\_] kPa psi.

#### 2.1.2.4 Polyvinylidene Fluoride (PVDF) Pipe and Tubing

PVDF pipe, tubing and fittings shall be manufactured from materials conforming to ASTM D 3222 for type II homopolymers. Pipe tolerances for outside diameter and wall thickness shall be in accordance with ASTM D 1785 for schedule 80 pipe. Tubing and associated fittings shall be rated for a minimum working pressure of [\_\_\_\_\_] kPa psi.

#### 2.1.2.5 Copper Pipe

Pipe 100 mm 4 inch and smaller shall be standard weight, seamless, cold drawn type conforming to ASTM B 88M ASTM B 88 Type K, temper H. Fittings shall be cast or wrought copper alloy, solder joint type, conforming with ASME B16.18 or ASME B16.22, as appropriate. Solder used shall be lead free and comply with ASTM B 32, grade Sb5, 95-5 tin-antimony or Sn96, 96-4 tin-silver solder.

#### 2.1.3 Pipe Hangers and Supports

Pipe hangers and supports shall conform to MSS SP-58 and MSS SP-69.

#### 2.1.4 Stainless Steel Gas Tubing and Fittings

Stainless steel tubing shall conform to ASTM A 778. Wall thicknesses shall be a minimum of 1.5 mm 0.062 inches for tubing 250 mm 10 inches and smaller, tubing 300 mm 12 inches in diameter shall have a minimum wall thickness of 1.9 mm 0.078 inches, tubing 350 through 450 mm 14 through 18 inches in diameter shall have a minimum wall thickness of 2.7 mm. 0.109 inches. Fittings shall conform to ASTM A 774/A 774M, and be of the same material, grade, schedule or wall thickness as specified for tubing. Joints shall be full penetration butt welded joints or Van Stone type joints using angle face rings with bracing flanges drilled in accordance with ASME B16.5.

#### 2.1.5 Valves

##### 2.1.5.1 Liquid Oxygen (LOX)

LOX valves shall be bronze or Type 316 stainless steel intended for cryogenic extended service. Materials shall be compatible with the piping installed.



#### 2.1.5.2 Gate

Gate valves shall comply with the requirements of Section 15400A PLUMBING, GENERAL PURPOSE.

#### 2.1.5.3 Ball

Ball valves shall comply with the requirements of Section 15400A PLUMBING, GENERAL PURPOSE. Valves used for hydrogen peroxide service shall be passivated and vented in accordance with the hydrogen peroxide supplier recommendations.

#### 2.1.5.4 Check

Check valves shall comply with the requirements of Section 15400A PLUMBING, GENERAL PURPOSE.

#### 2.1.6 Injectors

\*\*\*\*\*

NOTE: Designer should coordinate pressure requirements with equipment manufacturers to determine if supplemental pumping is required to ensure adequate gas transfer. In certain situations, multiple injectors may be required if large flow variations are expected. Injectors are most commonly used on smaller applications such as multiple columns in series where ozone can be injected to the individual columns.

\*\*\*\*\*

High efficiency venturi type injectors shall be constructed of 316L stainless steel or PVDF at a rated pressure of [\_\_\_\_\_] kPa psi. Each unit shall have a liquid flow capacity of [\_\_\_\_\_] L/s gpm, and shall be capable of applying 150 percent of the design gas flow of standard [\_\_\_\_\_] L/minute cubic feet/hour of a [\_\_\_\_\_] percent ozone in [air] [oxygen] mixture. Injectors shall be designed to operate with an available pressure head to the injector of [\_\_\_\_\_] kPa psi, and a back pressure of [\_\_\_\_\_] kPa psi.

#### 2.1.7 Diffusers

\*\*\*\*\*

NOTE: Designer should coordinate with diffuser manufacturers to determine the proper flow rate and coverage per diffuser. Rod type diffusers are generally used on larger rectangular tanks versus the dome or disc type which can be used in either circular reactors, or on rectangular units.

Coordinate access requirements with paragraph AOP Reactor Vessel.

\*\*\*\*\*

Fine bubble diffusers shall be ceramic construction, of the tube, disc or dome type. Ceramic shall be of bonded silica or alumina, and be resistant to degradation by ozone in oxygen concentrations of [16] [\_\_\_\_\_] percent. Pore size shall be a maximum of [50] [\_\_\_\_\_] um [0.002] [\_\_\_\_\_] inch or the manufacturer's standard pore size which will produce bubbles [2] [\_\_\_\_\_] mm [0.005] [\_\_\_\_\_] inches in diameter or smaller. Gas flow per diffuser shall

be a maximum of standard [\_\_\_\_\_] L/s cubic feet/minute at a submergence of [\_\_\_\_\_] meters feet. Maximum allowable headloss per diffuser shall be limited to [\_\_\_\_\_] mm inches. Brackets, holders, bolts, rods, washers and other accessories shall be 316 stainless steel unless otherwise indicated. Gaskets shall be of silicone construction.

#### 2.1.1.8 Couplings

Fittings, flanges, bolts, nuts and washers shall be the same material as the piping unless otherwise indicated. Sleeve type couplings for ozone service shall be of stainless steel conforming with ASTM A 312/A 312M, Grade TP316L with ozone resistant gaskets. Couplings for non-ozone ferrous metal piping shall be ASTM A 53/A 53M, Grade B.

#### 2.1.1.9 Insulating Joints

Insulating joints shall be provided when ferrous metal piping is joined with non-ferrous metal piping, fitting or valve materials. Insulating flanges shall be installed and have insulating flange gaskets, insulating sleeves for studs, and insulating washers for both sides of flanges. Steel washers shall be installed between the insulating washers and nuts. Couplings shall be of the same pressure rating as the pipe installed.

#### 2.1.1.10 In Pipeline Static Mixers

\*\*\*\*\*  
NOTE: Static mixers are generally recommended to ensure complete mixing when peroxide is used. Static mixers may also be needed in other processes in the treatment train; if so, coordinate and list those requirements separately or coordinate them with other specification sections to ensure there is no duplication.  
\*\*\*\*\*

In pipeline static mixers shall be installed [at the locations indicated] [upstream of the reaction chamber]. Mixers shall be [installed in a flanged section of piping] [with removable mixing sections] [inserted into the pipeline], have a pressure rating equal to that of the piping installed, have a maximum headloss of [\_\_\_\_\_] mm inches of water, [at [\_\_\_\_\_] L/s gpm] while inducing completely turbulent mixing conditions in the pipeline installed. Mixers [and housing] shall be constructed of [Grade 316 stainless steel] [\_\_\_\_\_] and be compatible with [hydrogen peroxide] [\_\_\_\_\_] [The static mixer shall be ported for direct application of the applied chemical.]

#### 2.1.1.11 Bolts, Nuts, Anchors and Fasteners

Bolts, nuts, anchors and fasteners shall be stainless steel in conformance with ASTM F 593.

### 2.2 MANUFACTURED UNITS

\*\*\*\*\*  
NOTE: Edit the following paragraphs to reflect the type of ozone generator feed gas (air or oxygen) that is included in the design package. A cost comparison should be performed prior to selecting the feed gas. Typically, oxygen in a liquid form or

generated onsite from ambient air will be used. Air feed ozone generators typically produce ozone concentrations of approximately 2 percent in air, while oxygen feed systems typically produce ozone concentrations of 6 percent or greater in oxygen. VSA systems are generally used for systems that generate greater than 900 kg (2000 pounds) per day.

For liquid oxygen (LOX) tanks, smaller than the minimum capacity stated in NFPA 50, state that the requirements indicated in the standard are to be applied to the tank size specified. LOX tanks should not be located inside a treatment facility. This paragraph contains statements describing a complete manufactured unit, usually a standard catalog item; statements may include descriptive requirements for the materials, specific fabrication, finishes, and function. Separate paragraphs for each different item should be used when appropriate. The name used for the manufactured unit must be consistent throughout the specification.

Generally, skid mounted equipment is preferred; however, this may not be possible with larger oxygen generation units (greater than 225 kg (500 pounds) per day). Verify dimensions with manufacturers to ensure the skid mounted units are transportable and do not have an excessively large space requirement over equipment that is field assembled. The following paragraphs may need to be modified to allow assembly, wiring, and plumbing in the field.

Additional information is contained in ETL  
1110-1-161.

\*\*\*\*\*

#### 2.2.1 Swing Adsorption Oxygen Generation System

The Oxygen Generation System shall be Swing Adsorption type. [Pressure swing adsorption (PSA)] [Vacuum swing adsorption (VSA)] system equipment shall be a complete unit process, including the compressor, [particulate filters,] [aftercooler separator,] heat exchangers, switching valves, instrument air dryer, adsorbent beds, adsorbent material, [oxygen receiver,] controller and other equipment as required by the manufacturer to provide a complete and operational oxygen generation system. [The unit] [Each component] shall be completely wired requiring only [interconnecting wiring between components] [an external connection for a single external power supply and remote monitoring] [and control] be done in the field. [PSA] [VSA] system equipment shall include all work from the outside air inlet to the ozone generator inlet connection. The [PSA] [VSA] system shall be a continuous output system with the following characteristics:

|                                 |  |
|---------------------------------|--|
| Min. oxygen generation capacity | [_____] kg/day lbs/day                           |
| Oxygen purity (minimum)         | [90] [_____] percent                             |
| Temperature to generator (max.) | [30] [_____] degrees C<br>[86] [_____] degrees F |



generally be less than 515 kPa (75 psi); significant cost savings can be achieved by reducing the tank pressure requirements, but lower pressure tanks may require a longer lead time to procure since the 1.2/1.7 MPa (175/250 psi) tanks are most commonly provided.

\*\*\*\*\*

Bulk LOX storage tanks shall be [\_\_\_\_\_] kg pound double walled vertical tanks constructed in conformance with [ASME BPVC SEC VIII D1] [\_\_\_\_\_] , rated for a maximum operating pressure of [1.2] [\_\_\_\_\_] MPa [175] [\_\_\_\_\_] psi and design temperature between minus 212 and plus 65 degrees C minus 350 and plus 150 degrees F, and seismic parameters defined in previous paragraph. The inner wall shall be constructed of [Grade 304 stainless steel] [9 percent nickel steel] [\_\_\_\_\_] , the outer shell shall be constructed of carbon steel with a minimum outer shell thickness of [10] [\_\_\_\_\_] mm [0.375] [\_\_\_\_\_] inches. Annular area between the inner and outer walls shall be insulated to limit oxygen boil off rate to less than [0.25] [\_\_\_\_\_] percent of the tank capacity per day at the maximum ambient conditions. Piping shall be copper or 316 stainless steel. Fittings shall be bronze or 316 stainless steel.

#### 2.2.2.2 Vaporizers

\*\*\*\*\*

NOTE: Vaporizers should be designed for the anticipated flow rate to the ozone generator. If vaporizers are oversized, gas temperatures will reach outside ambient temperatures, resulting in higher oxygen gas temperatures during the summer months being fed to the ozone generator, reducing its efficiency. Normal operating pressure for an ozone generator is approximately 103 kPa (15 psi). Resulting pressure at the diffusers is approximately 103 kPa (15 psi) less system losses.

In cold climates, heaters may be required to warm the oxygen gas feed to the ozone generator. The actual heating requirements should be coordinated with the ozone generator manufacturer. In cases where ambient temperatures fall below freezing for extended periods, supplementary heating may be necessary.

LOX systems may require a small quantity of nitrogen gas be added to the feed stream to facilitate ozone gas flow through the generator. This may be accomplished by adding a small volume of dried ambient air (about 2 percent).

\*\*\*\*\*

Vaporization equipment shall consist of a minimum of [2] [3] ambient air vaporizers and [single] [double] regulator system complete with automatic switching and a manual bypass. Each vaporizer shall be rated for 100 percent capacity, under continuous operation at a [\_\_\_\_\_] cubic meters per second SCFM withdrawal rate and also capable of supplying a peak withdrawal rate of [\_\_\_\_\_] cubic meters per second scfm. The vaporization equipment shall be designed for an inlet pressure of [\_\_\_\_\_] kPa psi, and a maximum headloss between the tank and ozone generator of [\_\_\_\_\_] kPa psi. The

vaporizer extrusions shall have extra wide spacings between the individual extrusions with a minimum area per extrusion of [1.65] [\_\_\_\_\_] square meters/meter [5] [\_\_\_\_\_] sf/ft. [Heaters shall be provided to automatically warm the oxygen feed gas to the ozone generator when the oxygen feed temperature falls to less than [\_\_\_\_\_] degrees C F. Heaters shall be capable of warming the oxygen feed gas to a temperature range between [10 and 22] [\_\_\_\_\_] degrees C [50 and 72] [\_\_\_\_\_] degrees F]. Each vaporizer shall operate for a minimum of [8] [\_\_\_\_\_] hours at the minimum ambient conditions and continuous withdrawal rate specified. The defrost cycle for each vaporizer shall be a maximum of [8] [\_\_\_\_\_] hours at the minimum ambient conditions and continuous withdrawal rate specified. Piping between the LOX tank and ozone generator shall be insulated as specified in Section 15080A THERMAL INSULATION FOR MECHANICAL SYSTEMS.

#### 2.2.2.3 Regulators

Regulators shall be factory tested with outlet pressure field adjustable over a downstream pressure range from [69 to 172] [\_\_\_\_\_] kPa [10 to 25] [\_\_\_\_\_] psi, from 0 to 100 percent of the specified oxygen flow rate. Regulators shall be rated at 1030 kPa 150 psi, and constructed of 316 stainless steel.

#### 2.2.3 Ozone Generator Air Feed System

System equipment which processes ambient air directly as the ozone generator feed gas shall be provided by a single supplier, [be of the pressure swing type and] include an air compressor and receiver, aftercooler, [refrigerative dryer], vapor/liquid separator, [coalescing and] [particulate] filters, desiccant air dryer, particulate after filter, switching valves, pressure, temperature and moisture monitors, local controller and other equipment as required by the manufacturer to provide a complete and operational air preparation system. [The equipment shall be skid mounted.] Adsorption vessels shall be designed and constructed in accordance with ASME BPVC SEC VIII D1. Adsorption material shall be [activated alumina] [\_\_\_\_\_] . The unit shall be completely wired requiring only an external connection for a single external power supply and remote monitoring [and control]. The air preparation system supplier shall be responsible for all work from the outside air inlet to the ozone generator inlet connection. The air preparation system shall be a continuous output system with the following characteristics based on 100 percent relative humidity and maximum ambient temperature of [\_\_\_\_\_] degrees C F:

|   |  |
|---|--|
| Minimum dry air feed to ozonator                    | [_____] cms scfm/m                               |
| Operating pressure at stated capacity               | [345] [_____] kPa<br>[50] [_____] psi            |
| Pressure drop through desiccant dryers<br>(maximum) | [20] [_____] kPa<br>[3] [_____] psi              |
| Maximum air temperature to ozone generator          | [30] [_____] degrees C<br>[86] [_____] degrees F |
| Maximum dewpoint (below 0 degrees)                  | [60] [_____] degrees C<br>[76] [_____] degrees F |
| Maximum hydrocarbon concentration                   | [0] [1] [_____] ppm                              |
| Discharge pressure to ozone generator (min)         | [_____] kPa psi                                  |

|                             |   |
|-----------------------------|---|
| Cycle time adjustable range | [1 to 5] [_____] minutes                  |
| Power supply                | [480] [_____] volt,<br>3 phase, 60 hertz. |

#### 2.2.4 Ozone Generator System

\*\*\*\*\*

**NOTE:** Delete this paragraph if an ozone generator is not used. Horizontal tube, medium frequency generators are the most common; however, since the state of the art is constantly changing, verify that other types of generators are not available or appropriate for the particular application.

Coordinate pressure requirements with paragraph Air Feed System. Typical pressure ranges required for ozone systems are dependant upon the final ozone outlet pressure, generally between 69 and 103 kPa (10 and 15 psi) plus losses through the equipment.

\*\*\*\*\*

Ozone generation equipment shall be continuous duty water cooled, multi-tube glass or non-glass multitube dielectric [horizontal tube] [vertical tube] assemblies contained in a pressure vessel [with hinged gas-tight doors] with a rated design pressure of [\_\_\_\_\_] kPa psi. Each unit shall be provided with [medium] [high] frequency electrical power supply units including input and output transformers, power controller, frequency inverter, harmonic mitigation equipment (if required). The generator shall be provided with complete controls, [compatible with the central control unit,] instrumentation, panels, appurtenances and miscellaneous equipment required for a complete ozone generating system using [oxygen] [air]. All equipment, valves, piping, associated appurtenances shall be suitable for ozone in [oxygen] [air] service. Generator design requirements are as follows:

|   |  |
|---|--|
| Capacity  | [_____] kg lbs per day                           |
| Gas flow rate to generator  | [_____] cms scfm                                 |
| Outlet pressure $\pm$ 5 %)  | [_____] kPa psi                                  |
| Ozone concentration   | [_____] percent                                  |
| Generator vessel design pressure                                      | [_____] kPa psi                                  |
| Ozone output concentration turn down                                  | [10:1] [_____]                                   |
| Cooling water temperature rise at rated production capacity (maximum) | [3] [_____] degrees C<br>[5] [_____] degrees F   |
| Carrier gas rise across generator (max.)                              | [30] [_____] degrees C<br>[17] [_____] degrees F |
| Inlet hydrocarbon concentration (max)                                 | [0] [_____] ppm                                  |
| Power supply  | [480] [_____] volt, 3 phase,<br>60 hertz.        |

#### 2.2.4.1 Ozone Generator Vessels

All ozone generator metal parts which come into contact with ozone or cooling water shall be constructed of Type 316L stainless steel. The vessel shall be designed to resist an internal pressure of 1.5 times the design pressure, including the tubes and shell. Over pressure protection based on worst case operating conditions shall be provided. The vessels shall be constructed in accordance with ASME BPVC SEC VIII D1 code. Viewing ports shall be provided to allow visual inspection of all internal dielectrics during operation.

#### 2.2.4.2 Dielectric Tubes

Dielectric tubes shall be constructed to resist thermal shock and to evenly distribute the applied electrical charge over the entire dielectric surface without arcing. Dielectric tubes shall be formed from either glass or a non-glass material with a certified voltage breakage strength of 1.5 times the maximum possible operating voltage under maximum temperature and applied power conditions. Dielectric tubes shall be protected by fuses or functionally equivalent devices to prevent shorting dielectric tubes from damaging the shell and tube structure in the ozone generator.

#### 2.2.5 Ozone Destruct System

\*\*\*\*\*

**NOTE: High concentrations of chlorinated organics may be liberated by systems which use ozone in air or oxygen. These chlorinated organics may "poison" a catalyst bed designed only for ozone destruction. If considerable concentrations of chlorinated organics are anticipated (greater than 1000 ppm) in the reactor off gas, a chlorine resistant catalyst should be specified or a separate specification section should be used.**

\*\*\*\*\*

Ozone off gas destruction equipment shall be thermal assisted catalyst destruct type units suitable for moist ozone in [oxygen] [air] service. The catalyst containment unit, piping, ductwork, and other metallic components shall be constructed of 316 stainless steel. The units shall be capable of destroying contactor off gas generated by the ozone generators which feed the AOP reactors. The ozone destruction unit shall have the capability to function at a minimum turn down ratio of 20 to 1. Each off gas destruction unit shall be a skid mounted unit consisting of [a demister,] an electric resistance heater, catalyst trays and containment vessel [, and a centrifugal blower]. The destruction unit discharge duct shall be sloped away from the destruct unit to reduce the probability of catalyst fouling from condensation. Ducts carrying ozone laden off gas from the AOP reactors shall be sloped to a low point valved drain located upstream of the ozone destruct system. The ozone destruct system shall reduce the ozone concentration from the off gas flow to less than [0.10] [\_\_\_\_\_] ppm by volume of ozone from zero flow to the maximum off gas flow rate. Normal operation is defined as [50] [\_\_\_\_\_] percent of the maximum off gas flow rate with an ozone concentration of [1.0] [\_\_\_\_\_] percent by weight. Ozone destruction equipment shall meet the following requirements:

|  |                         |
|--|-------------------------|
| Maximum pressure drop through catalyst | [_____] mm of mercury   |
| at maximum flow rate                   | [_____] inches of water |



|   |  |
|---|--|
| Maximum pressure drop through heater at maximum flow rate | [ ] mm of mercury<br>[ ] inches of water     |
| Maximum off gas relative humidity                         | [ ] percent                                  |
| Maximum temperature rise across heater                    | [20] [ ] degrees C<br>[35] [ ] degrees F     |
| Catalyst chamber empty bed contact time                   | [1.0] [ ] seconds                            |
| Max. ozone concentr. into destruct unit weight            | [1.0] [ ] percent by weight                  |
| Off gas flow rate (maximum)                               | [ ] cubic m/s<br>[ ] scfm                    |
| Maximum catalyst bed temperature                          | [120] [ ] degrees C<br>[250] [ ] degrees F   |
| Off gas temperature to catalyst bed                       | [15] [ ] degrees C<br>[60] [ ] degrees F     |
| Power supply  | [480] [ ] volts,<br>[3] [ ] phase, 60 hertz. |

The catalyst shall be non-hazardous [manganese dioxide/copper oxide] [nickel] [ ] based material suitable for catalytic ozone destruction at the specified conditions. The catalyst containment unit shall be provided with a flanged and bolted top or hatch a minimum of 300 mm 12 inch in diameter to facilitate change out of the catalyst material when the catalyst is exhausted.

#### 2.2.6 Hydrogen Peroxide System

\*\*\*\*\*

**NOTE:** Edit Section 11242A CHEMICAL FEED SYSTEMS to provide on-off, set point, or proportional control as appropriate.

Hydrogen peroxide storage system requirements should be coordinated with suppliers to ensure material compatibility. Floating roof manway area should equal 1 in 2 per 400 L (100 gallons) for solutions less than 52 percent, and 2 in 2 per 400 L (100 gallons) for solutions greater than 52 percent. Process safety management requirements must be followed any time more than 3375 kg (7500 pounds) of H2O2 is stored, or the solution strength is greater than 52 percent; refer to 29 CFR 1910.119 for information.

Hydrogen peroxide storage tanks should be located outside when possible. Polyethylene should not be used for peroxide concentrations greater than 52 percent.

\*\*\*\*\*

The hydrogen peroxide storage tank shall be constructed of cross linked polyethylene, 316 stainless steel, or 99.5 percent pure aluminum alloys designated in [ASTM B 209M] [ASTM B 209] as 1060, 5254, 5652. Hydrogen peroxide storage tanks shall be provided with secondary containment [as detailed on the drawings] [\_\_\_\_\_] with a minimum capacity equal to [110] [\_\_\_\_\_] percent of the maximum storage tank volume. Hydrogen peroxide storage tanks shall be equipped with [50] [\_\_\_\_\_] mm [2] [\_\_\_\_\_] inch female quick fill connection; [600] [\_\_\_\_\_] mm [24] [\_\_\_\_\_] inch hinged, weighted and gasketed manway cover; [50] [\_\_\_\_\_] mm [2] [\_\_\_\_\_] inch filtered breather vent; liquid level site tube; and [600] [\_\_\_\_\_] mm [24] [\_\_\_\_\_] inch free floating roof manway cover. All piping connections shall be flanged. Feed pumps shall conform to the requirements of Section 11242 CHEMICAL FEED SYSTEMS.

#### 2.2.7 Redox Potential Meter

The oxidation reduction meter shall be provided [where indicated on the drawings] [on the effluent line of each reactor]. Probe shall be easily removable without interrupting service. Probe materials shall be resistant to ozone as well hydrogen peroxide attack over a pH range of 2 to 12 and operating pressures of up to [\_\_\_\_\_] kPa psi and suitable for a temperature range from [0 to 100] [\_\_\_\_\_] degrees C [32 to 212] [\_\_\_\_\_] degrees F and suitable for the medium monitored. Probe shall transmit output to an ORP analyzer with digital output. The ORP analyzer shall transmit a [[4 to 20] [\_\_\_\_\_] mA signal proportional to the ORP] [direct digital reading] to the central control unit.

#### 2.2.8 pH Probe

The pH probe shall be provided [where indicated on the drawings] [on the effluent line of each reactor]. Probe shall be easily removable without interrupting service. Probe materials shall be resistant to ozone as well hydrogen peroxide attack over a pH range of 0 to 14 and operating pressures of up to [\_\_\_\_\_] kPa psi and suitable for a temperature range from [0 to 100] [\_\_\_\_\_] degrees C [32 to 212] [\_\_\_\_\_] degrees F and suitable for the medium monitored. Probe shall transmit output to a pH analyzer with digital output. The pH analyzer shall transmit a [[4 to 20] [\_\_\_\_\_] mA signal proportional to the pH] [direct digital reading] to the central control unit.

#### 2.2.9 Ozone Monitors

##### 2.2.9.1 Vapor Phase

Separate ozone monitors shall be provided to monitor ozone in ambient air, [at the locations shown on the drawings,] determining the ozone levels downstream of the off gas ozone destruct system, [and the ozone concentration in the ozone generator discharge]. The ambient air monitoring unit intake shall be located [within 455 mm 18 inches above the treatment plant floor] [at the location shown on the drawings] [adjacent to the AOP process equipment]. The ambient air monitors shall be interlocked with the ozone generation system to initiate an alarm condition, and ozone generator shut down when readings exceed preset levels. Analyzers shall be [4 to 20 mA] [direct digital] output ultraviolet adsorption photometer type with built in pressure and temperature compensation. Ozone off gas monitor shall have a minimum of five separate ranges to monitor concentrations between [[0 to 15] [\_\_\_\_\_] percent,] [[0 to 99,000] [\_\_\_\_\_] ppm by volume]. Ambient air and off gas destruct monitors shall have a minimum of five separate ranges to monitor concentrations between [0 to 10] [\_\_\_\_\_] ppm.

Each monitor shall be provided with a builtin digital ozone concentration readout at the unit.

#### 2.2.9.2 Liquid Phase

Liquid phase monitors shall be provided [where indicated on the drawings] [on the effluent line of the last reactor]. Sensor shall transmit output to an ozone analyzer with digital display and remote signal transmission to the central control unit. Probe shall transmit output to a liquid phase ozone analyzer with digital output. The liquid phase ozone analyzer shall transmit a [[4 to 20] [\_\_\_\_\_] mA signal proportional to the ozone concentration] [direct digital reading] to the central control unit.

#### 2.2.10 Temperature Sensors

Temperature sensors shall be dual switch trip point independently adjustable type with a minimum accuracy of 0.5 percent of full scale. Thermal system shall be constructed of 316L stainless steel. Temperature range shall be from [0 to 100] [\_\_\_\_\_] degrees C [32 to 212] [\_\_\_\_\_] degrees F and suitable for the medium monitored. Sensor shall transmit output to an analyzer with digital output. The analyzer shall transmit a [[4 to 20] [\_\_\_\_\_] mA signal proportional to the temperature] [direct digital reading] to the central control unit.

#### 2.2.11 Compressors

Air compressors shall conform to ASME B19.3. Air compressors shall be factory packaged [rotary screw] [centrifugal] [rotary] [reciprocating] type units. The air compressors shall be packaged in an enclosure with sound attenuating properties which allow a maximum noise level measurement of 75 dBA at the equipment enclosure. Air compressors shall be [water] [air] cooled and rated for continuous operation. Guards shall shield exposed moving parts. Compressor motors and starters shall conform with the requirements of Section 16402 INTERIOR DISTRIBUTION SYSTEM. Air compressors shall have the manufacturer's name and address, together with trade name, and catalog number on a nameplate securely attached to the equipment. Any special maintenance instructions (required before startup or shutdown) shall be included in the Operations and Maintenance Manuals. Compressor equipment used for processing ambient air for the ozone generator feed gas shall include the air compressor, receiver with automatic condensate drain, intake air filter and silencer, after cooler, a high efficiency moisture separator, [refrigerative dryer], pressure, temperature and moisture monitors, local controller and other equipment as required by the manufacturer to provide a complete and operational oil free, dry compressed air system. Compressor receivers, air piping, valves and appurtenances unless otherwise specified, shall be in conformance with Section 15400A PLUMBING, GENERAL PURPOSE. Dry contacts and 4 to 20 mA signals shall be provided in the control panel for remote monitoring.

|   |  |
|---|--|
| Minimum capacity  | [_____] cms scfm                                 |
| Operating pressure at stated capacity                   | [345] [_____] kPa<br>[50] [_____] psi            |
| Maximum air temperature to PSA/VSA system               | [30] [_____] degrees C<br>[86] [_____] degrees F |
| Maximum dewpoint to PSA/VSA system<br>(below 0 degrees) | [60] [_____] degrees C<br>[76] [_____] degrees F |

Maximum hydrocarbon concentration [0] [\_\_\_\_\_] ppm  
Cycle time adjustable range [1 to 5] [\_\_\_\_\_] minutes

#### 2.2.12 Blowers

Blowers shall conform to [Section 11215 FANS/BLOWERS/PUMPS; OFF-GAS] [\_\_\_\_\_] . Dry contacts and 4 to 20 mA signals shall be provided in the control panel for remote monitoring.

#### 2.2.13 Dew Point Monitor

The dew point transmitter shall be of a solid state design housed in a NEMA 4 enclosure as defined in NEMA 250, with an accuracy of plus or minus 3 degrees C over an operating ambient temperature range of minus 10 to plus 60 degrees C, over a dew point range of minus 110 to plus 10 degrees C. The transmitter shall receive the signal from the thin film aluminum metal oxide sensor, convert and send it as a [single 4 to 20 mA DC signal proportional to the dewpoint level] [direct digital reading] to the central control unit. Sensor shall transmit output to an analyzer with digital display.

#### 2.2.14 Pressure Gauges

Water pressure gauges shall be glycerine filled units conforming to the requirements of ASME B40.100.

#### 2.2.15 Sampling Ports

Aqueous and gas phase sampling ports shall be provided [where indicated on the drawings] [upstream and downstream of each reactor vessel]. Sampling ports shall be provided at locations accessible to plant operators. Ports and associated piping shall be constructed of [6] [12] [\_\_\_\_\_] mm [1/4] [1/2] [\_\_\_\_\_] inch minimum diameter [PVDF] [316 stainless steel] [teflon] [\_\_\_\_\_] with [PVDF] [316 stainless steel] [\_\_\_\_\_] [NPT x hose] ball valves.

#### 2.2.16 Gas Flow Meters

\*\*\*\*\*  
**NOTE: Numerous meters may be required which may necessitate a table be included identifying the flow capacity for each unit.**  
\*\*\*\*\*

Flow meters for ozone or oxygen applications shall have stainless steel body, tube, valves, floats, and knobs with glass windows. Flow meter shall be rated for a flow rate of [\_\_\_\_\_] cms scfm at a minimum pressure of [345] [\_\_\_\_\_] kPa [50] [\_\_\_\_\_] psi. Each flow meter shall be provided with a separate stainless steel valved connection for ease of maintenance. Each pipe penetration through the reactor wall serving a single ozone diffuser or bank of diffusers shall be equipped with a flow meter. The [air] [oxygen] feed stream to the ozone generator shall also be equipped with a flow meter. Each flow meter shall have an easily readable scale in cms scfm with a minimum of ten divisions from zero to 150 percent of the expected flow through the meter. Each meter shall be provided with an analyzer which receives the signal from the flow meter transmitter, converts and sends it as a [single 4 to 20 mA DC signal proportional to the flow rate] [direct digital reading] to the central control unit. Sensor shall

transmit output to an analyzer with digital display.

#### 2.2.17 Level Monitoring

Pressure type level sensors, associated analyzers and transmitters shall be provided for each liquid process tank associated with the AOP system. Sensor element shall be removable for servicing or replacement without taking the tank out of service. As a minimum, the following tanks shall be equipped with level monitoring equipment: [reactor vessels,] [hydrogen peroxide storage and feed tanks,] [equalization tank,] [effluent storage and equalization tanks,] [\_\_\_\_\_]. Each level control element shall be of solid state design constructed of materials compatible with the liquid stored. Each controller shall be provided with an analyzer which receives the signal from the level sensor, converts and sends it as a [single 4 to 20 mA DC signal proportional to the liquid level] [direct digital reading] to the central control unit.

#### 2.2.18 Reactor Vessel

\*\*\*\*\*

NOTE: Coordinate paragraph Gas Flow Meters requirements for the application; indicate penetration requirements, if a packing support is required; view ports; site glasses; or material options to stainless steel reactors. Also include access requirements for removal and maintenance of diffusers. Coordinate unique concrete material ozone resistance requirements with Section [03300A CAST-IN-PLACE STRUCTURAL CONCRETE] [03300N CAST-IN-PLACE CONCRETE] if concrete reactor vessels are used.

Reactors for peroxone systems, where either the ozone or hydrogen peroxide dose is not expected to exceed 25 ppm, may be constructed of fiberglass if appropriate resins are used. Coordinate with tank suppliers regarding specification requirements.

\*\*\*\*\*

The reactor vessel shall be [circular] [rectangular], fabricated of [316L stainless steel] [concrete conforming to Section [03300A CAST-IN-PLACE STRUCTURAL CONCRETE] [03300N CAST-IN-PLACE CONCRETE] [\_\_\_\_\_] provided with [\_\_\_\_\_] mm inch, [\_\_\_\_\_] kPa psi flanged connections.] Reactor vessels shall have a minimum water depth above the diffusers of [6] [\_\_\_\_\_] m [18] [\_\_\_\_\_] feet, with a minimum free board water depth above the liquid level of 600 mm 2 feet. [Reactor shall be designed to accommodate a vacuum of [25] [\_\_\_\_\_] mm [1] [\_\_\_\_\_] inch applied to the reactor headspace.] Welding shall be performed in accordance with AWS D1.1/D1.1M by welders certified to have passed qualification tests using procedures covered in AWS B2.1 or ASME BPVC SEC IX. Reactors shall be equipped with openings required to ensure maintenance and installation/removal of the following equipment: liquid inlets and outlets, gas inlet supply and off gas collection points, sampling connections, [quartz sheath wipers], [UV lamps], [pH probe], [redox meter], [level switch], site glass liquid level indicator, and other connections as indicated or required. Reactor vessels shall be equipped with a minimum of [one] [\_\_\_\_\_] viewing port no smaller than [0.5] [\_\_\_\_\_] m [1.5] [\_\_\_\_\_] feet located [0.7] [\_\_\_\_\_] m [2] [\_\_\_\_\_] feet minimum above the bottom of the reactor. The viewing port shall be covered with clear plastic material not susceptible to ozone degradation,

with a minimum thickness of [10] [\_\_\_\_\_] mm [3/8] [\_\_\_\_\_] inch.

## 2.3 ELECTRICAL

Electrical products shall be in accordance with Section 16402 INTERIOR DISTRIBUTION SYSTEM. Reactor vessels containing ultraviolet lamps shall be independently grounded.

### 2.3.1 Motors

Motors, all motor starters, and any control or signal wiring required for the operation of the specified equipment shall be provided and installed under this section in accordance with Section 16402 INTERIOR DISTRIBUTION SYSTEM unless otherwise specified herein, in other sections, or indicated on the drawings.

### 2.3.2 Local Controls and Panels

Manual or automatic controls, protective or signal devices required for the operation specified, and any control wiring required for controls and devices, shall be provided. Enclosures for local power and control panels shall conform to NEMA ICS 6.

### 2.3.3 Ultraviolet Equipment Electrical Requirements

- a. A separate prewired power panel shall be provided for each module.
- b. Ground fault detection or independent ground shall be standard with the UV lamp equipment.
- c. Control and monitoring components shall be housed in NEMA enclosures. Internal components shall be sealed from the environment. System electronics to be used in an interior environment shall be housed in enclosures conforming to NEMA 250 TYPE 12. System electronics to be used in an exterior and corrosive environment, as defined in NEMA 250, shall be housed in enclosures conforming to NEMA 250 TYPE 4X.
- d. Sufficient cooling shall be provided to the medium and high temperature UV bulbs as well as associated ballasts to prevent overheating.
- e. Wiring and electrical connections shall be protected against moisture and corrosive gases to prevent electrical shorts or failure. Electrical installation and materials shall conform to NFPA 70. The unit shall be completely wired requiring only an external connection for a single external power supply and remote monitoring and control.
- f. Interconnecting, multiconductor, unshielded cables shall be suitable for outdoor installation. Insulation shall be thermoplastic rubber with an operating range of minus 60 to 125 degrees C minus 75 to 260 degrees F with low temperature flexibility and flame retardants. UV stabilized jacketing shall be resistant to oils, chemicals, fuels, solvents, and to mechanical abuse and abrasion. Cable shall be supplied by the equipment manufacturer and shall be of sufficient length and number for a complete system.

- g. Cableways provided shall be stainless steel, 1.98 or 1.59 mm 14 or 16 gauge thick.

## 2.4 AOP CONTROL SYSTEM

\*\*\*\*\*

NOTE: Delete items within this paragraph that do not apply. Not all UV systems (especially those with low intensity lamps) have light intensity monitors; verify design requirements for type or need of lamps. Hydrogen peroxide monitoring on all but very large plants (larger than 1.5 MGD) will consist of tank level readings and an indication that the chemical feed pump is working. Coordinate with paragraph Alarms and Interlocks if separate audible or visual alarms beyond the control system specified are required, and their location.

If an autodialer is required, reference the controls and instrumentation section of the specification; or if none is included and an autodialer is required, include those requirements in this paragraph.

\*\*\*\*\*

Equipment shall be locally controlled and shall be capable of receiving standard digital or analog control signals from the plant central control system. Status and adjustments to the equipment shall be provided [locally] [and] [from the plant central control system]. Instruments shall be provided with mounting hardware as appropriate. Transmitters with digital outputs shall be accurate to within [\_\_\_\_\_] percent. All equipment shall be designed for operation on a 120 volts 60 hertz electrical input. Controls shall be provided to remotely monitor [and adjust] [hydrogen peroxide delivery rate,] [oxygen] [air] [and ozone output,] [\_\_\_\_\_] [individual lamp failure,] [power on and off status for each lamp [ballast]] [ultraviolet lamp intensity]. [Each lamp shall be provided with a nonresettable elapsed time meter with ability to record operable hours from 0 to 99,999].

### 2.4.1 Ozonation Control System

The ozonation control system shall be interfaced with the plant central control system. Changes to the ozone generator equipment operating conditions shall be accomplished locally or from the master control panel. The power, control and instrumentation system provided shall be as specified or as recommended by the ozone generator manufacturer for safe operation and supervision of the ozone generator and related gas feed equipment. Schematics and interconnecting wiring diagrams shall be provided for power, control, and instrumentation circuits. Control power transformers, relays, adjustable timers, auxiliary contacts, switches, or additional equipment to interconnect the generator to other auxiliary equipment and master control panel, and control circuits as shown on schematic or instrument control drawings shall be provided. An emergency stop button shall be provided at the local generator control panel. The ozone generator shall be protected from power surges, and variations in power supplied to the equipment.

### 2.4.2 Hydrogen Peroxide Feed

\*\*\*\*\*

NOTE: Hydrogen peroxide metering rate is generally done manually with an interlock to shut the system down when a flow switch or other interlock at the AOP master control indicates a flow interruption. If a variable flow rate is anticipated, although rarely used, the hydrogen peroxide feed rate can be tied to the influent meter or AOP master control. Coordinate operation with Section 11242A CHEMICAL FEED SYSTEMS.

\*\*\*\*\*

Hydrogen peroxide feed pump and control shall conform to the requirements of Section 11242 CHEMICAL FEED SYSTEMS.

#### 2.4.3 Alarms and Interlocks

\*\*\*\*\*

NOTE: Delete items in this paragraph that are not required.

Coordinate this paragraph with process and instrumentation diagrams (PIDs) and other specification sections. Metering accuracy for hydrogen peroxide is generally done manually. Indicate if separate audible or visual alarms beyond the AOP master control system are required, and their location.

\*\*\*\*\*

Alarms and interlocks shall be provided to ensure proper operation of the advanced oxidation equipment, and its sequenced shutdown based on potentially unsafe or improper conditions that may exist. The following paragraphs list alarms that (as a minimum) shall be monitored at the central control point, or that will initiate shutdown of the appropriate advanced oxidation equipment components.

##### 2.4.3.1 AOP System

Failure of major equipment components such as lamps, ballasts, or safety interlocks shall initiate system, followed by plant shutdown, if not acknowledged. AOP system alarms and control interlocks shall be provided for the following items:

- Lamp failure
- Ballast failure
- Safety interlocks for open door on reactor vessel or panel
- High water temperature in AOP reactor vessel
- Low water flow to the reactor vessel
- Sleeve wiper failure
- High pressure in reactor vessel headspace
- [\_\_\_\_\_].

##### 2.4.3.2 Metering Pump

Pump failure shall initiate system, followed by plant shutdown, if not acknowledged. Metering Pump alarms and control interlocks shall be provided for the following items:

- Hydrogen peroxide feed



Catalyst feed  
Pump failure  
[\_\_\_\_\_].

#### 2.4.3.3 Hydrogen Peroxide Tank

Hydrogen peroxide tank [alarms] [and control interlocks] shall be provided for the following items:

High liquid level  
Low liquid level  
Low low liquid level  
High temperature  
High pressure  
[\_\_\_\_\_].

#### 2.4.3.4 Ozone System

Ozone system alarms and control interlocks shall be provided for the following items:

High dew point in gas feed to ozone generator  
Over current to the power supply unit (PSU)  
Over voltage to the PSU, rectifier, and inverter  
Over frequency protection  
High temperature shut down  
High inlet gas temperature  
High inlet cooling water temperature  
High gas pressure to the generator  
Insufficient gas flow to the generator  
High outlet ozone gas temperature  
High moisture level in control cabinet  
[\_\_\_\_\_].

Major equipment component failure such as over current, over voltage, over frequency, high cooling water temperature or other condition that could damage the equipment or result in effluent non-compliance shall initiate system, followed by plant shutdown, if not acknowledged.

#### 2.4.3.5 Gas Feed System

Gas feed system alarms and control interlocks shall be provided for the following items:

High pressure across gas filters  
High temperature in gas desiccant dryer  
High pressure downstream of reducing valves  
Air preparation system failure  
Ozone monitor failure  
[\_\_\_\_\_].

Major equipment component failure, such as high cooling water temperature, air preparation failure, or other condition that could damage the air feed or ozone equipment, or result in effluent non-compliance shall initiate system, followed by plant shutdown, if not acknowledged.

#### 2.4.3.6 Ozone Destruct System

Ozone destruct system alarms and control interlocks shall be provided for

the following items:

- High ozone in ambient air space
- High gas flow rate to destruct unit
- Low temperature in ozone destruct unit
- High ozone in destruct unit exhaust gas
- Ozone destruct system failure
- High ozone concentration in off gas
- Destruct system failure
- [\_\_\_\_\_].

Health and safety ambient ozone level non-compliance shall initiate ozone system alarm and shutdown, followed by overall plant shutdown, if alarm is not acknowledged (high ambient ozone levels will not shutdown the ozone destruct system concurrently with other processes).

#### 2.4.3.7 Cooling Water System

Cooling water system alarms and control interlocks shall be provided for the following items:

- Cooling systems failure
- High water temperature
- No/low cooling water flow
- Pump failure
- [\_\_\_\_\_].

Major equipment component failure such as no/low cooling water flow, pump failure or other condition that could damage the gas feed, ozone equipment or result in effluent non-compliance shall initiate ozone generator, followed by plant system shutdown, if not acknowledged.

#### 2.4.3.8 Metering Accuracy

Metering accuracy alarms and control interlocks shall be provided for the following items:

- Ozone
- Hydrogen Peroxide

#### 2.4.3.9 Ground Fault

A ground fault protection alarm shall be provided.

### 2.5 SPECIAL EQUIPMENT AND TOOLS

One set of special tools, calibration devices, and instruments required for operation, calibration, and maintenance of the equipment shall be provided. The Contractor shall provide a tube cleaning rack or racks with adequate capacity to hold [50] [100] percent of the dielectric tubes from the ozone generator being serviced. Each rack shall be equipped with locking casters to allow the rack to be easily moved between the ozone generator and the location where the dielectric tube cleaning will occur. Each dielectric shall be provided with an individual padded holder.

## PART 3 EXECUTION

### 3.1 EXAMINATION

The equipment installation shall be as indicated on the drawings, shop drawings, manufacturer's instructions and recommendations. The limits of work for the equipment supplied shall be compared to field conditions to ensure the limits previously identified for piping, electrical and control interfaces meet the actual physical requirements at the facility. Any discrepancies shall be brought to the attention of the Contracting Officer for correction.

### 3.2 PREPARATION

\*\*\*\*\*  
**NOTE: This paragraph covers actions required to  
physically prepare the surface, area, or site to  
incorporate the specified primary products.**  
\*\*\*\*\*

The reactor vessel, [ozone and feed gas equipment,] [hydrogen peroxide storage and feed system,] [electrical support equipment,] and [\_\_\_\_\_] shall be provided with an equipment pad isolated from the floor slab [as detailed on the drawings] [adequate to properly support the equipment]. Reinforced concrete shall be designed and installed in accordance with Section [03300A CAST-IN-PLACE STRUCTURAL CONCRETE] [03300N CAST-IN-PLACE CONCRETE]. Prior to placing ozone piping, or other equipment, into service it shall be cleaned by one of the methods specified in CGA G-4.1. Piping and equipment used to store or feed hydrogen peroxide shall be passivated in accordance with the hydrogen peroxide supplier's requirements.

### 3.3 PIPES, VALVES, FITTINGS AND APPURTENANCES

Piping, valves, fittings, and appurtenances shall be installed in accordance with the manufacturers recommendations, as specified in Section 15400A PLUMBING, GENERAL PURPOSE, or as otherwise indicated. All valves, fittings, meters and other appurtenances shall be given unique identification numbers corresponding to those used in operation and maintenance manuals, and in AOP submittals prepared. Identification numbers shall be placed on brass identification tags and securely fastened to all valves, fittings, meters and other appurtenances. Tags shall not be less than 38 mm 1-1/2 inches in diameter with depressed black figures 13 mm 1/2 inch high. Piping for wet ozone service shall be PVDF, stainless steel, or PTFE. Piping for dry ozone service shall be PVDF, stainless steel, or PTFE. Oxygen Piping shall be copper or stainless steel. Hydrogen peroxide piping shall be stainless steel, PTFE or PVDF. Oxygen piping shall [be insulated in accordance with Section 15080A THERMAL INSULATION FOR MECHANICAL SYSTEMS] [not be insulated].

### 3.4 ELECTRICAL WORK

Electrical work shall be in accordance with the drawings and applicable requirements of Section 16402 INTERIOR DISTRIBUTION SYSTEM. Equipment shall be appropriate for continuous duty, and installation in a dusty, humid and corrosive environment. Electrical equipment and wiring shall comply with NFPA 70.

### 3.5 TOOLS

Tools shall be provided to the Contracting Officer prior to the onsite training identified in paragraph FIELD TRAINING.

### 3.6 PAINTING/CORROSION PROTECTION

All ferrous surfaces shall be coated or painted. Color shall be as indicated on the paint schedule or as otherwise approved. Factory painted items shall be touched up as needed. Factory painted items requiring touch up in the field shall be thoroughly cleaned of all foreign material, primed and top coated with the manufacturer's standard factory finish in accordance with the manufacturer's recommendations, including dry finish thickness. Equipment which did not receive a factory finish shall be painted in accordance with the requirements indicated in Section 09900 PAINTS AND COATINGS. Painting corrosion resistant metals such as brass, bronze, aluminum, copper, galvanized steel and stainless steel is not required unless otherwise specified.

### 3.7 CHEMICALS

\*\*\*\*\*  
**NOTE: Coordinate these requirements with other specifications which may address extended operation and maintenance occurring in some HTRW Projects. If other supplies such as catalysts are required, include that information as well.**  
\*\*\*\*\*

The Contractor shall provide the chemicals needed to do all the operational and start up testing, and shall completely refill the [oxygen], [hydrogen peroxide], [catalyst], [\_\_\_\_\_] tanks at the time of contract completion.

### 3.8 WELDING

\*\*\*\*\*  
**NOTE: Use second set of brackets when critical pipe welding is required.**  
\*\*\*\*\*

[Piping shall be welded in accordance with qualified procedures using performance qualified welders and welding operators. Procedures and welders shall be qualified in accordance with ASME BPVC SEC IX. Welding procedures qualified by others, and welders and welding operators qualified by another employer may be accepted as permitted by ASME B31.1. The Contracting Officer shall be notified 24 hours in advance of tests. Structural members shall be welded in accordance with Section 05090A WELDING, STRUCTURAL.] [Welding and nondestructive testing procedures for piping shall be as specified in Section 05093 WELDING PRESSURE PIPING.]

### 3.9 SAMPLING AND ANALYSIS

Sampling, analysis, and sample turn around time to demonstrate system performance and effluent compliance shall be performed in accordance with Section 01450A CHEMICAL DATA QUALITY CONTROL. A commissioning/demonstration plan shall be prepared and submitted for approval to ensure the equipment meets the standards indicated. The plan shall include calculations and a detailed description of proposed sampling and analysis required to document system performance. The contractor shall

coordinate this plan with other plans and unit operations to ensure they do not conflict and the AOP system is ready for testing. The contractor shall coordinate and obtain regulatory approvals prior to notifying the contracting officer that the equipment is ready for testing. The chemical parameters identified in Paragraph: Performance Requirements [and ambient and ozone off-gas destruction concentrations] shall be sampled [daily] [\_\_\_\_], monitored [at the locations identified on the drawings] [at the locations indicated in the startup/commissioning plan] for [7] [\_\_\_\_] days of continuous 24 hour operation, using analyses with detection limits one order of magnitude lower than the levels indicated in Paragraph: Performance Requirements.

### 3.10 FIELD TESTS AND INSPECTIONS

\*\*\*\*\*

**NOTE: These tests are required for installed or completed work; they are different and separate from those required for materials and products prior to installation or application. Delete tests not applicable or required.**

**Provide in this section a reference to the plant commissioning or start-up specification which includes the processes in the treatment facility.**

\*\*\*\*\*

Accessories such as the [UV equipment,] [ozone generator,] [compressor,] [ozone generator gas feed equipment,] and [\_\_\_\_] shall be factory tested prior to shipment to the job site.

#### 3.10.1 AOP Reactor Vessel

The AOP reactor vessel and attached appurtenances shall be assembled at the factory and an operational test of all components accomplished prior to shipment. Certification that the equipment and components assembled at the factory are operational and meet the specification requirements shall be provided to the Contracting Officer a minimum of [10] [\_\_\_\_] calendar days prior to shipment. Components not assembled at the factory shall be subject to the same tests and inspections prior to onsite leak testing using potable water. Following installation at the project site, and prior to leak testing, the AOP system shall be retested to ensure the equipment and auxiliary components act as a complete and operational system. This shall include operation of all valves, pumps, blowers, analyzers, alarms, meters, interlocks, monitors, level and pump controls, sensors, switches, off gas destruct equipment and all other equipment associated with the AOP system. Testing shall be completed prior to leak testing and written notification provided to the Contracting Officer stating the equipment is working in accordance with the contract documents and manufacturer's recommendations prior to the commencement of leak testing.

#### 3.10.2 Diffuser or Injector System

The entire gas piping system shall be pressure tested with dry air or oxygen at a minimum of [two] [\_\_\_\_] times the normal design pressure for a minimum of 60 minutes and such additional time as required for the Contractor to inspect the piping system for leaks. All leaks shall be repaired and the system shall be retested until no leakage is detected. Ozone shall not be introduced into the system until all leaks have been identified, repaired, and the system retested. [Diffusers] [Injectors]

shall be installed in accordance with the suppliers recommendations. After installation, the [diffusers] [injectors] shall be covered with clear water to a depth of approximately [1] [\_\_\_\_\_] m [3] [\_\_\_\_\_] feet. Dry air or oxygen shall be released through the [diffusers] [injectors] and the system shall be inspected for uniform air or oxygen distribution throughout the reactors. Following the initial testing at [1] [\_\_\_\_\_] m [3] [\_\_\_\_\_] feet, the distribution testing shall be repeated at a water depth of [3] [\_\_\_\_\_] m [9] [\_\_\_\_\_] feet to ensure bubble distribution is adequate throughout the reactor. [Diffuser] [Injector] replacement or repositioning shall be accomplished as required to maintain uniform air distribution throughout the reactor. If after repositioning, air distribution throughout the reactor lacks uniformity, additional redistributors or deflectors shall be installed in the reactor as recommended by the [diffuser] [injector] supplier to accomplish uniform flow distribution throughout the reactor.

### 3.10.3 Leak Testing

Leak testing shall be accomplished at the factory to verify the integrity of the reactor vessels and associated gas and liquid piping. The factory leak test shall be accomplished on the reactor vessel and appurtenances following assembly at the factory. Onsite hydrostatic leak testing shall include all piping between the upstream and downstream processes, and be accomplished using potable water at a pressure 1.5 times the working pressure, or 350 kPa 50 psi unless otherwise approved by the Contracting Officer. The reactor vessel and appurtenances shall be isolated from the connecting piping and retested for leaks using potable water following assembly at the site. The ozone generator gas connections shall be tested with dry air or oxygen at the maximum pressure allowed by the manufacturer, or as identified in the previous paragraph. Any gas or liquid leaks identified during the aforementioned testing shall be repaired and the system shall be retested until the systems are free of leaks.

### 3.10.4 Control Panel

A local control panel functionality test shall be performed and approved by the Contracting Officer prior to commencement of leak testing or testing using oxidizers. The central control testing shall be accomplished prior to overall plant startup.

### 3.10.5 Ozone Generation System

\*\*\*\*\*

**NOTE: The installer or manufacturer should demonstrate the operation and efficiency of the equipment. Power consumption for ozone generation should be less than 10 kWhr per 0.5 kg (pound) of ozone generated assuming a PSA oxygen feed system is used to generate a 10 percent ozone feed; verify this with multiple equipment suppliers based on the specific ozone application pressures to be used, gas feed, and applied ozone concentration.**

\*\*\*\*\*

The ozone generation system shall be tested to ensure that the actual ozone production, power usage, or water consumption rates meet recommended requirements. Power usage shall be measured after achieving steady state conditions as determined by the ozone generator supplier. Power usage shall be measured at the central motor control center or at each individual component including the [air dryer,] [refrigerant driers,] [desiccant

driers,] [oxygen generator,] ozone generator, cooling water pumps, and master control panel. Power usage shall be within [5] [\_\_\_\_\_] percent of [\_\_\_\_\_] kWh per kg pound of ozone generated at 100 percent of rated capacity. Cooling water supply shall also be measured. Cooling water consumption rate shall not exceed [\_\_\_\_\_] L/s gpm at the parameters listed in paragraph Ozone Generator by more than [5] [\_\_\_\_\_] percent. If the equipment does not meet the specified consumption rates, the Contractor shall make the necessary system revisions to meet the rates specified at no additional cost to the Government. Power usage shall also be evaluated at 25, 50, and 75 percent of the design production rate.

### 3.11 MANUFACTURER'S SERVICES

\*\*\*\*\*

**NOTE: Use this paragraph when manufacturers are to provide field quality control with onsite personnel for instruction/supervision of the installation or application of their products, or for startup or demonstration.**

**This paragraph covers requirements of the installer or manufacturer to demonstrate the operation and maintenance of equipment to the owner's personnel.**

\*\*\*\*\*

The manufacturer shall provide a qualified service representative experienced in the installation, adjustment, operation and maintenance of the equipment specified for a minimum of [3] [\_\_\_\_\_] days. The representative shall supervise the installation, adjustment, testing, and shall provide instruction in the operation, and maintenance of the equipment. If major components from multiple suppliers are provided, such as an [ozone generator] [air preparation system] [oxygen preparation system] [ozone destruct system] [\_\_\_\_\_] , each supplier shall be required to visit the site a minimum of [1] [\_\_\_\_\_] times during equipment installation or startup. During the startup and [one] [\_\_\_\_\_] years operating period, the major equipment suppliers shall be required to be onsite [2] [\_\_\_\_\_] times to verify that the equipment is installed and operates properly, and to provide trouble shooting and technical assistance.

### 3.12 FIELD TRAINING

A field training course shall be provided for designated operating and maintenance staff members. The training shall include operation of individual components as well as the integrated system, maintenance needs and procedures, instrument calibration, safety issues and emergency procedures, control and alarm features, troubleshooting equipment and control problems, and laboratory analytical procedures. Training shall be provided during normal working time and shall start after the system is functionally complete but prior to performance testing. Field training shall cover all of the items contained in the operating and maintenance manuals. Each major equipment vendor including, but not limited to, the ozone generator, ozone destruct system, ozone monitoring system, and gas feed system shall be required to provide two [8] [\_\_\_\_\_] hour periods of classroom and hands-on operating instruction to the individuals selected by the Contracting Officer. The first period shall be at system startup and the second [as defined by the Contracting Officer] [at the end of the Contractor's operating contract, prior to turning over to the long term facility operator].

### 3.13 MAINTENANCE

#### 3.13.1 Maintenance Service

\*\*\*\*\*  
NOTE: Delete this paragraph if UV lamps are not used. The designer may want to provide additional information regarding lamp change out if the system is limited to a certain lamp type. Medium pressure lamps have an approximate life of 3 to 4000 hours, while low pressure lamps have an approximate life of 7 to 10000 hours; certain proprietary, high intensity lamps may have a life less than 2000 hours.  
\*\*\*\*\*

The Contractor shall be responsible for changing out lamps, ballasts, and quartz tube wipers at the frequency recommended by the manufacturer during the one year warranty period or as otherwise required. Lamps and ballasts supplied as specified below, shall be provided in addition to the complete set supplied for installation (following the warranty period) and those installed as needed during the warranty period. The ozone generator dielectrics shall be cleaned in accordance with the manufacturer's recommendations immediately prior to the conclusion of the Contractor's operating period; or after one year, if greater than one year after startup, and at the conclusion of the Contractor's operating period.

#### 3.13.2 Extra Materials

\*\*\*\*\*  
NOTE: Delete inapplicable portions of these paragraphs. Coordinate this section with other sections of the specifications to ensure there are not conflicts regarding supplying consumables. Verify the duration of the initial operating period, which is generally 1 year.  
\*\*\*\*\*

The Contractor shall furnish the initial supplies to fill the vessels, as well as all consumables during the startup, prove out, and initial operation period. At the time the Contractor turns the plant over to the long term Operation and Maintenance Contractor, the vessels storing consumables such as LOX, hydrogen peroxide [and] [\_\_\_\_\_] shall be refilled within [two] [five] days prior to the plant turn over.

##### 3.13.2.1 Lamps

The Contractor shall provide a complete set of lamps that shall be reserved for change out by the equipment supplier following the one year warranty period. This extra set of lamps shall be delivered to the treatment facility 60 days prior to the end of the one year warranty period and installed by the Contractor. Lamp replacement during the one year warranty period shall be provided by the supplier, as needed by the Contractor.

##### 3.13.2.2 Spare Parts

The supplier shall provide, in addition to the lamps specified above, a minimum of ten percent of each of the following items, or a minimum of two, whichever is greater:



- a. Lamp ballasts
- b. Quartz sleeves
- c. End seals
- d. Socket connectors
- e. O-rings
- f. Quartz sleeve cleaners
- g. Diffusers
- h. Rotometers
- I. Generator dielectrics
- j. Generator dielectric fuses
- k. pH probe element
- l. ORP probe element

#### 3.14 POSTING FRAMED INSTRUCTIONS

Framed instructions containing wiring and control diagrams, under glass or in laminated plastic, shall be posted adjacent to the equipment or where otherwise directed. Condensed operating instructions, prepared in typed form, shall be framed as specified above and posted beside the diagrams. The framed instructions shall be posted before acceptance testing of the system.

-- End of Section --